Integrating Biotechnology and Nanotechnology into Sustainable Industrial Complexes



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Organization of Material

- Introduction to Sustainable Development
- Introduction to Biotechnology
 - Feedstock
 - Processes
 - Products
- Introduction to Nanotechnology
 - Carbon nanotubes
- Integration of biotechnology and nanotechnology in existing plant complex
- Research Direction

Carbon Dioxide

Annual average fossil carbon dioxide emissions:1990s:23.5 GtCO2 (6.4 GtC) per year2000-2005:26.4 GtCO2 (7.2 GtC) per yearGlobal atmospheric concentration:650,000 years:180-300 ppm2005:379 ppmAnnual carbon dioxide concentration growth-rate:1960 = 2005 average:1.4 ppm per year1995 = 2005 average:1.9 ppm per year

IPCC WGI Fourth Assessment Report, 2007

Global Warming Radiative Forcing Surface Climate Temperature



Photo: National Geographic, October 2007

Sustainable Development

What can we do with the CO_2 ?

- Reduce its emission by increasing efficiency and conservation
- Carbon capture and storage
- Low carbon fuels
- Use renewable feedstock
- Utilize CO₂ to make chemicals

This introduces us to the concept of "Sustainable Development"

Development that meets the needs of the present without compromising the ability of future generations to meet their own needs – United Nations Department of Economics and Social Affairs, Division for Sustainable Development

Industries in Louisiana

Petrochemical complex in the lower Mississippi River Corridor



Photo: Peterson, 2000

Sustainability

Sustainability refers to integrating development in three aspects

- Economic
- Environmental
- Societal

There are numerous approaches to attempt an integration of these aspects by world organizations, countries and industries.



Corporate Sustainability

• A company's success depends on maximizing the profit as expressed below.

Profit = Σ Product Sales – Σ Raw Material Costs – Σ Energy Costs

- The profit equation above can be expanded to meet the **"Triple Bottomline"** criteria of sustainability.
- This will incorporate the economic costs expanded to environmental costs and societal costs (also referred to as the sustainable or sustainability costs)
 - Triple Bottom Line = Σ Product Sales + Σ Sustainable Credits
 - $-\Sigma$ Raw Material Costs $-\Sigma$ Energy Costs
 - Σ Environmental Costs Σ Sustainable Costs

Triple Bottom Line = Profit – $\Sigma Environmental Costs + \Sigma Sustainable (Credits – Costs)$

Achieving the Goal





841,118 million cubic feet NG in 2006

80% increase in NG price from 2001 to 2005

Increases the cost of raw material

Results in plant shutdown or relocation



Research Vision

- Propose a biomass based chemical industry in the chemical production complex in the Gulf Coast Region and the Lower Mississippi River Corridor.
- Propose the production of **carbon nanotubes** in the complex.
- Utilize all **carbon dioxide** from all processes in the complex to make chemicals.
- Assign costs to the **Triple Bottomline Equation** components.
- Propose a Mixed Integer Non-Linear Programming problem to maximize the Triple Bottomline based on constraints: multiplant material and energy balances, product demand, raw material availability, and plant capacities
- Use Chemical Complex Analysis System to obtain Pareto optimal solutions to the MINLP problem
- Use Monte Carlo simulations to determine sensitivity of optimal solution

Components





Oil





Lignocellulosics

- Switchgrass
- Sugarcane Bagasse
- Corn Stover
- Agricultural residues

Separate and extract hexose and pentose



Cellulose, Hemicellulose and Lignin





Photo: LSU AgCenter, 2006; National Geographic, October 2007



Urban Wood Waste

Waste Biomass

- Municipal Solid Waste
- Animal Manures
- Food Processing Wastes
- Wood and residues from pulp and paper mills
- Logging residues



Sugarcane Bagasse



Logging Residue

• Algae

- Consumes CO₂ in a continuous process using exhaust from power plant (40% CO₂ and 86 % NO)
- Can be separated into oil and carbohydrates
- High oil density yields production rate of **15,000 gallons/acre** compared to 60 gallons/acre for soybeans
- Water used can be recycled and waste water can be used as compared to oilseed crops' high water demand
- High growth rates, can be harvested daily

Use Algae to consume CO₂ from production processes
Algae becomes feedstock for the production of oil and carbohydrates for chemicals



Photo: National Geographic, October 2007

Feedstock in Louisiana



Biomass Processes

The following biomass conversion processes are planned for integration into the chemical complex superstructure:

- Fermentation
- Anaerobic digestion
- Transesterification
- Gasification
- Direct conversion of plant oils

Pretreatment of biomass is necessary before any of the biomass conversion processes.

- Pretreatment
 - Physical size reduction biomass is cut into pre-determined sizes for feeding into pretreatment reactors.
 - Hot wash releases the complex structure of the biomass components releasing the cellulose, hemicellulose and lignin.
 - Acid hydrolysis dissolves hemicellulose into pentose oligomers. Also forms degradation products under severe conditions.
 - Enzymatic hydrolysis breaks down cellulose to C6 sugars (hexoses) and hemicellulose to C5 sugars by yeast or bacteria containing the enzyme (cellulase or hemicellulase).
 - Oil extraction this process extracts oil from oil seeds for further processing

Breaks complex starch, cellulose and hemicellulose structures to glucose and pentose. Removes lignin from the process.

Fermentation

- Fermentation is the enzyme-catalyzed transformation of an organic compound.
- Fermentation enzymes react with hexose and pentose to form products.
- Enzyme selection determines product :-
 - Saccharomyces Cervisiae (C6), Escherichia coli (C5 & C6), Zymomonas mobilis (C6)– Ethanol
 - Engineered Eschericia coli, A. succiniciproducens Succinic Acid
 - Engineeried microorganism Butanol
 - Lactic Acid Producing Bacteria (LAB) Lactic Acid



Anaerobic Digestion

- Anaerobic digestion of biomass is the treatment of biomass with a mixed culture of bacteria in absence of oxygen to produce methane (biogas) and carbon dioxide.
- Four stages: hydrolysis, acidogenesis, acetogenesis and methanogenesis
- MixAlco process Inhibits fourth stage of methane production using iodoform (CHI₃) or bromoform (CHBr₃). Reduces cost of process by using mixed culture of bacteria from cattle rumen. Produces mixed alcohols, carboxylic acids and



Direct Conversion of Plant Oils

- Plant oils can undergo transesterification or epoxidation.
- Hydroformylation of methyl esters followed by hydrogenation gives monomer for polyols.



Transesterification

- Transesterification process is the treatment of vegetable oil with an alcohol and a catalyst to produce esters and glycerol.
- Methanol or ethanol is used as alcohol for fatty acid methyl or ethyl esters (FAME/FAEE).
- These esters can be transformed to chemicals.
- Glycerol is produced ~ 10% by weight in the process.
- Glycerol can be introduced to the propylene chain



Gasification

- Production of syngas
- Syngas can be converted to chemicals like methanol, ammonia and hydrogen





New Products from Biomass











Carbon Nanotubes

- Seamless cylindrical tubes, consisting of carbon atoms arranged in a regular hexagonal structure
- Consist of carbon filaments with nanoscale (10⁻⁹ m) diameter and micron scale (10⁻⁶ m) length.
- Considered as the ultimate engineering material because of their unique and distinct electronic, mechanical and material characteristics.

- Challenges
 - Production of purified carbon nanotubes in commercial quantities at affordable prices.
 - Equivalent quantity of carbon dioxide produced.
 - Market price is \$100-\$400/gm for purified nanotubes and \$1500-\$2000/gm for electronics grade CNT.
 - Bayer is building a 3,000 mt/yr plant from a 60 mt/yr capacity to produce carbon nanotubes (Baytubes[®])



Conceptual Design of CNT Processes

	CNT PFR Process	CNT-FBR Process
Catalyst	Fe	Co – Mo
	$Fe(CO)_5 \rightarrow Fe + 5CO$	Silica
Reactants	CO and Fe(CO) ₅	СО
Reactor Type	Plug Flow Reactor	Fluidized Bed
Reactor Conditions	1050 °C @ 450 psi	950 °C @ 150 psi
Selectivity to CNT	90%	80%
Purification	- Oxidation	- Leaching
	- Acid Treatment	- Froth Flotation
	- Filtration	- Acid Treatment
Production rate (kg/hr)	595	595
Production rate (kg/hr)	595	595





Integrated Chemical Production Complex



Base Case of Plants in the Lower Mississippi River Corridor







Research Directions

Extend the Chemical Production Complex in the Lower

Mississippi River Corridor to include:

Biomass based chemical production complex

Carbon Nanotube production in the complex

 CO_2 utilization from the complex

Obtain the relations for the above chemical plants:

Availability of raw materials

Demand for product

Plant capacities

Material and energy balance equations

Assign Triple Bottomline costs:

Economic costs

Environmental costs

Sustainable credits and costs

Research Directions

- Define Multicriteria Optimization Problem with constraints
- Use Mixed Integer Non Linear Programming Global Optimization and Local Optimization Solvers to obtain Pareto optimal solutions of the problem below.
 - GAMS/BARON Global Optimizer
 - GAMS/DICOPT Local Optimizer

w_1P+w_2S

 $P = \Sigma Product Sales - \Sigma Economic Costs - \Sigma Environmental Costs$

 $S = \Sigma Sustainability (Credits - Costs)$

$w_1 + w_2 = 1$

- Use Monte Carlo Analysis to determine sensitivity of the optimal solution.
- Follow the procedure to include plants in the Gulf Coast Region (Texas, Louisiana, Mississippi, Alabama)
- Methodology can be applied to other chemical complexes of the world.



Questions

Comments

